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## **AMENDMENTS TO THE CLAIMS**

This listing of claims will replace all prior versions and listings of claims in the application:

## LISTING OF CLAIMS:

1. (currently amended): A cyclone system for disengaging solid and gaseous particles which is in association with a FCC processes with reduced reactor and which reduces coke formation in a disengager vessels vessel that receives a catalyst/load mixture from a riser, comprising at least one legless cyclone [[42]] connected to at least one cyclone [[47]] in consecutive stages through concentric pipes 46a, 46b, wherein the system has a at least one legless cyclone [[42]] is fitted with at least one collector pipe [[43]] outside the at least one legless cyclone [[42]].

- 2. (currently amended): The system of claim 1, wherein it the system reduces coke formation inside the disengager vessels vessel without causing spent catalyst to be released inside the system.
- 3. (currently amended): The system of claim 1, wherein it-the system maintains the overall efficiency of the disengagement and the integrity of the cyclones during run time.
- 4. (currently amended): The system of claim 1, wherein the at least one collector pipe [[43]] is positioned outside to keep the spent and previously disengaged catalyst from being released into the cyclones in consecutive stages.
- 5. (currently amended): The system of claim 1, wherein <u>the</u> at least one collector pipe [[43]] has a device of a suitable shape at its end to keep the spent and previously disengaged catalyst from being released into <u>the</u> at least one cyclone [[47]] in consecutive stages.

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6. (currently amended): The system of claim 1, wherein the <u>a</u> connection between the <u>concentric</u> pipes 46a, 46b-that interconnect the cyclones in different and consecutive stages is fitted with a telescoping joint [[45]] with minimized annular space.

- 7. (currently amended): The system of claim 1, wherein as an alternative the a connection between the concentric pipes 46a, 46b interconnecting the cyclones in different and consecutive stages is fitted with a sealed telescoping joint.
- 8. (currently amended): The system of claim 1, wherein as an alternative the a connection between the concentric pipes 46a, 46b-interconnecting the cyclones in different and consecutive stages has no telescoping joint.
- 9. (currently amended): The system of claim 1, wherein the <u>a</u> lower nozzle of the <u>at</u> least one legless cyclone [[42]] is fitted with distributors [[42a]] of solids.
- 10. (currently amended): The system of claim 1, wherein the <u>a</u> lower nozzle of the <u>at</u> least one legless cyclone [[42]] has no distributors of solids.
- 11. (currently amended): The system of claim 1, wherein it-the system comprises at least one flow distributor [[46]] between cyclones in the same stage.
- 12. (currently amended): The system of claim 1, wherein it-the system comprises at least one flow distributor [[46]] between cyclones in different stages.
- 13. (currently amended): The system of claim 1, wherein it-the system has no flow distributors [[46]] between cyclones in equal stages.

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14. (currently amended): The system of claim 1, wherein it-the system has no flow distributors [[46]] between cyclones in different stages.

- 15. (currently amended): The system of claim 1, wherein each stage comprises at least one external collector pipe[[ 43]].
- 16. (currently amended): The system of claim 1, wherein it—the system further comprises at least one purge liquid injector device[[ 40]].
- 17. (withdrawn-currently amended): A process for disengaging solid and gaseous particles in processes a process for the fluid catalytic cracking (FCC) of hydrocarbons, reducing which reduces coke formation in a disengager vessels vessel, by using the system in accordance with of claim 1, said process comprising the following steps:
- a) feeding a suspension made up of cracking reaction products mixed with the a catalyst in a closed-the cyclone disengaging system for fostering the disengaging of gaseous and particulate phases, with the a gaseous current flowing into the a fractionation system through an outlet duct[[48]];
- b) collecting the <u>a</u> particulate phase in the bottom of the disengager vessel [[ 49]], from where it flows to the <u>a</u> rectification and regeneration zone;
- c) purging the stagnated areas of the disengager vessel [[49]] by injecting purge liquid through the an injector devices 40 device; and
- d) draining off the hydrocarbons recovered in the <u>a</u>rectifier and the steam injected into the disengager vessel and the rectifier, said process comprising the following:

wherein, in In-stage d), the gases coming from the disengager vessel [[49]] are drained off through the at least one collector pipe [[43]] outside the at least one legless cyclone[[42]],

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avoiding the passage of hydrocarbons into the top of the disengager vessel, with its which has a lower temperature[[;]], and

In-in stage b), a minimum of the catalyst disengaged through the lower nozzle of the <u>at least one</u> legless cyclone [[42]] is released by the gases drained off through the <u>at least one</u> external collector pipes 43 pipe.

- 18. (withdrawn-currently amended): The process of claim 17, wherein the at least one external-collector pipe [[43]] captures the gases coming from the disengager vessel[[49]], in a location close to the lower nozzle of the at least one legless cyclone[[42]], the at least one collector pipe [[43]] rising outside of and parallel to the at least one legless cyclone [[42]] and discharging the gases collected inside the concentric pipes 46a, 46b.
- 19. (withdrawn-currently amended): The process of claim 17, wherein the annular space of the concentric pipes 46a, 46b allows for potential thermal expansion of the system.
- 20. (withdrawn-currently amended): The process of claim 17, wherein a connection between the concentric pipes that interconnect the cyclones in different and consecutive stages is fitted with a telescoping joint, and the telescoping joint 45 between the concentric pipes 46a, 46b allows for thermal expansion of the system.
- 21. (withdrawn-currently amended): The process of claim 17, wherein any emmercially available an expansion joint allows for thermal expansion of the system.
- 22. (withdrawn-currently amended): The process of claim 17, wherein the process minimizes the route taken by hydrocarbons coming from the rectifier in the disengager vessel [[49]] until being captured by the <u>at least one collector pipes 43-pipe</u> and carried to the piping with an outlet above the at least one legless cyclone[[42]].

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23. (withdrawn-currently amended): The process of claim 17, wherein the process minimizes access by the hydrocarbons coming from the rectifier in the area of the disengager vessel [[49]] with having a lower temperature, which lies between the lower end of the at least one legless cyclone [[42]] and the top of the disengager vessel [[49]], whereby coke formation is reduced.

- 24. (withdrawn-currently amended): The process of claim 17, wherein the hydrocarbons coming from the rectifier are collected in a warmer area of the disengager vessel [[49]], thus preventing coke from being deposited in said disengager vessel.
- 25. (currently amended): The device system of claim 1, wherein the an upper end of said external the at least one collector pipe [[43]] opens up into the concentric pipes 46a, 46b, above the at least one legless cyclone[[42;]].
- 26. (currently amended): The <u>device-system</u> of claim 1, wherein <u>said-external-the at</u> <u>least one collector pipe [[43]] points vertically downward[[;]].</u>
- 27. (currently amended): The device-system of claim 1, wherein the a lower end of said external the at least one collector pipe [[43]] opens up into the disengager vessel [[49;]].
- 28. (currently amended): The <u>device-system of claim 1</u>, wherein <u>said external the at least one collector pipe [[43]] allows for various shapes that prevent the release of catalyst into the at least the one cyclone [[47]] in consecutive stages.</u>

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29. (withdrawn-currently amended): The device-system of claim 241, wherein at least one collector pipe [[43]] is installed in such a way as to keep the spent and previously disengaged catalyst from being released into the cyclones in consecutive stages.